

International Conference on Advanced Computer Science and Information System 2012 (ICACSIS 2014) Hotel Ambhara, Jakarta October 18th - 19th, 2014

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A Real Time Simulation Model of Production System of Glycerol Esterification With Self Optimization

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abstract— This paper presents a new approach af a Real Time Simulation (RTS) to model the Gycerol Esterification (GE) production system with Self Optimization(SO). The quality and capacity of production GE are the factors that need monitor and control. In this model, we deployed BPMN to analyze and design the requirement and used data acquisition system with real time sensor. Real-time data acquisition by optical sensors acquired several quality parameters such as viscosity, pH, purity and density which was interfaced to a SQL database. The model of selfoptimization for quality surveillance was based on previous Wagels (2012) work. The experiments showed that the evaluation of the system performance was operatable to optimize a range of parameter esterification with Oleic Acid in producing Glycerol Mono Oleate (GMO) such as temperature between at range of 240-260 °C, baffle rotation speed between at range 300-400 RPM and volume at range 25-30 L for each batch .The previous works only set in a fixed value at 250 °C,350 RPM and 24L. In future work, it is recommended to accelerate the whole process including to re-structure the real time data acquisition system.

Keywords: real time simulation; Glycerol Esterification (GE); self-optimization.

I. INTRODUCTION

The integration of advanced data acquisition for optimization and real time simulation offers considerable potential for innovations in the field of conventional production system. To increasing performance of system affected by many internal or external factors. An increase in the quality of the production system, which will secure sustained production for manufacturing companies, can thus be achieved [1]. Using SO on process level, for example can be used to calculate machine and process parameters online according to changing outer conditions [2]. In process production GE there exist

many possible scenarios how to solve these problems, but which of these scenarios is the best (optimal)? Is it possible to imagine how a change in the subsystem affects the entire system? , As one a product of agriindustrial sector, Glycerol as by product of biodiesel. The production of Biodiesel is still increase, as the result from the goverment policy that use it for mixed material for solar. Glycerol is an oil soluble food additive It is also used as an ingredient in the production of chewing gum and ice cream [3]. To produce Glycerol Esterification (GE) process that using raw material Crude Glycerol, there is small medium manufacturing that used conventional system and has many customer production requirements to make Glycerol Mono Oleate (GMO).

One of motivational example in optimization in GE production is such as follows : In conventional GE production system, the quality of product may vary from the customer requirement. It would affect to the unstable volume of production as this requirement observed and controlled manually. Our proposal for the optimization and simulation in a real time mode would enable for monitoring the flow of production and find the best parameter with SO. The mechanism of SO within the framework of RTS assumed each monitored parameters to a right adjustment.

The objective of these paper is to construct the model that applied the RTS method with SO. This method can be explained with BPMN diagrams, using sensors and data acquisition system and find the parameter of production that closely related to the quality of product and the volume target of production Glycerol Ester. In these paper for Section II we briefly explain description of problem. In Section III we briefly review the concept of SO in production system of GE. In Section IV we present analysis and design production system of GE. For Section V we make an experiment to compare the performance of system of the proposed method with the existing method and the conclusion are discussed in Section VI.

II. DESCRIPTION OF PROBLEM

System is an integrated set of interoperable elements that working synergistically to perform value-added processing and to satisfy the user with a specified outcome [4]. Every system consists of its inputs, entities, outputs, stakeholders, roles, constrains, etc that need to be identified. The quality and capacity of production are the problem that involve in production system in GE because of their variously characteristic for quality in end product that sometimes in a part of the product that not satisfy the customer . In this research we focused on production and quality control that dynamically changes by the factors like: material condition and capacity flow process for the process reaction. To optimize all that division we are using computer simulation in real time and to find the best configuration of production system with SO. In these paper we explained how to collect data set by system acquisition with sensors and flow measurement of the process to monitor and control the volume by using BPMN diagrams and using discrete and continuous (hybrid) modelling simulation computer software ARENA (Rockwell Automation Software Inc 2011) and interfaced with a SQL database.

III. SELF OPTIMIZATION CONCEPTS IN PRODUCTION SYSTEM

A.Production System of GE

The complexity of production system on production GE, we analyzed it by using Business Processing Modelling Diagram as in Fig 1, With this analysis, we can explain clearly the low level tasking in the production system that can improve the efficiency and effectiveness in the system [5] especially in order to produce the GE. The purity of glycerol obtained is low due to the presence of impurities such as remaining catalyst, water, soaps, salts and esters formed during the reaction [6]. The process of production GMO by reaction of Esterification that involving many parameter affected quality.

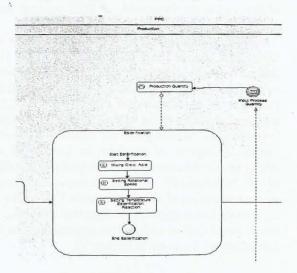


Fig 1.BPMN Esterification Process

B. Quality Control

In testing with FTIR, the method provides separation of acylglycerides, methyl and ethyl esters peaks. In was used C23:0 as internal standard. The method developed is faster and allows the elution of longchain triacylglycerides [7]. But in this research we are setup QC system using Mid IR optical source and detector for identification ethyl ester peaks to meet the quality needed for the customer in GMO production as in Fig.2.



Fig 2 .MID IR LED Optical Source

C. Self Optimization

In order to design production system with using the optimum parameter we are using SO and simulation with real time data acquisition method .The behavior of optimization algorithms is random, so we had to perform many optimization experiments to identify the pure nature of the optimization algorithms doing it by automatically as diagram in Fig. 3. By considering the number of simulation experiments we can divide the number of simulation experiments as follows:Simulation experiment –simulation run of simulation model.

- Optimization experiment –performed with concrete optimization method setting to find optimum of objective function.
- Series –replication of optimization experiments with concrete optimization method setting.

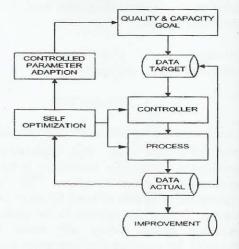


Fig.3. Self Optimization Process

We specified the same conditions to satisfies for each optimization method, e.g. the same termination criteria, the same search space where the optimization method can search for the global optimum

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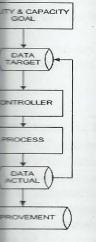


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system with using the SO and simulation method .The behavior indom, so we had to fiments to identify the gorithms doing it by By considering the ts we can divide the experiments as -simulation run of

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Process

tions to satisfies for the same termination here the optimization global optimum optimization method has the same parameters as optimization method, we set up both boundaries (same step, low boundaries). Self-optimizing systems are optimized by the interaction of contained elements and optimizing execution of the actions: [8]

continuous analysis of the current situation, in this markets parameter selected of pure gliserol

determination of quality targets of GE, production

Each production of the system's behavior to achieve these **argets like** temperature setting and rotational speed of **argets like** this paper we concerned to compare data **arget each** sampling. We assumed:

 $f_{min}=f_t-f_{(t-1)}$ (1) and for the object optimizing is O_i , the self optimizing open , can be formulated as:

 $O_{i \text{ avg }} \operatorname{opt}(P) \leftrightarrow (A)$ (2) **There P** is process, and A is attribute. In this case we **manalysis P** as $\{p_1, p_2, \dots, p_k\}$ and attribute as p_1, p_2, \dots, p_k and attribute as p_2, \dots, p_m . For Mathematical model of **MEEP**(feature selection) The weight of the i the **management** is then updated, the mathematical model is:

$$w_{i} = w_{i} + |x^{i} - NM^{i}(x)| - |x^{i} - NH^{i}(x)|$$
(3)

as we used in this research to find the parameter closely related to determined quality of GMO.

The development of a simulation of an actual seem involves the creation of a conceptual model of actual system to be simulated), which may be end on a set of rules, or a set of mathematical minors, or some other method of defining the state in simulation and and the way in which it changes time. A simulation based on a discrete model bishes an initial state of the system and a future queue with event timings. Event-based mulation in which time advances from event to event single software thread has been the basis of many pular discrete simulation languages, but, as parallel mulation in grant processors and multiple software threads become the more popular approach.

Deal Time Simulation

Real-time systems differ from traditional data ressing systems in that they are constrained by this nonfunctional requirements (e.g. dependability timing constraints or requirements). An efficient relation of real-time system requires a model that the both simulation objectives and timing results [9]. There is one research developed a relation for very detailed simulation models generation for very detailed simulation models foor control [10]. They identified two essential foor control [10]. They identified two essential to be automated for automatic simulation model relation: System specification and the associated construction. In this work, a proposed from a resource model as seen in Figure 4. This was made possible because the Arena simulation software supports Visual Basic Application (VBA), which enables application integration and automation. undertook the development of a modeling methodology to efficiently model real-time systems to satisfy given simulation objectives and to achieve arbitrary timing requirements.

In this paper we built the simulation of Manufacturing Systems is performed using RTS concept with Discrete and Continuous Event (Hybrid) Computer Simulation Program [11]. The Software for simulation we using ARENA Version 12 (Rockwell Ltd,2011)[12] with the schema in Fig.4 and real time data acquisition system with using flow sensor. The data was collected to SQL after the system of process has steady state condition.

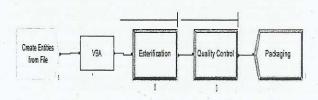
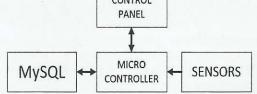
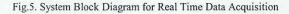


Fig.4 . Real Time Simulation Diagram of Production GE with ARENA

In this research we use field and data type for SQL as in Table I, and designed the system block for processing signal from sensors to interface with a SQL connection in this work we deployed MySQL (Oracle 2014)[13] by using Microcontroller as diagram in Fig 5.

Field	Data Type
Time	Time
Sensor 1.2 µm	Numeric
Sensor 3.4 µm	Numeric
Sensor 5.4 µm	Numeric
pH Sensor	Numeric
Viscosity Sensor	Numeric
Temperature	Numeric
Rotational speed	Numeric





E. Quality Control Factor Analysis

In this work, o analysis the factor that are related to quality control and for select the parameter we used RELIEF algorithm which are generalisable to polynomial classification by decomposition into a number of binary problems proposed by [14]. We used RELIEF to reduce unimportant features that result for a more efficient computation and sensor task. In order to propose some updates to the algorithm (RELIEF) to improve the reliability of the probability approximation and make it robust to incomplete data, and generalising it to two-class quality problems which is passed and not passed as in Fig. 6 and the selection attribute weighted as in Fig.7. In RELIEF classification we have collected 30 dataset being tested by the customer of GMO.

%Water	Viscosity (poise)	%FFA	рН	Purity	Rel.Density	Quality Pass
50	0.0514	30	7	70	0.95	NO
40	0.0500	50	7	80	0.98	YES
70	0.0456	20	6	50	0.96	NO
30	0.0514	- 60	7	90	1	YES
50	0.0534	70	8	70.	1.020	YES
40	0.0512	40	7	80	1.005	YES
80	0.0511	50	8	40	1.045	NO

Fig. 6. Sample Data Parameter for Quality Control

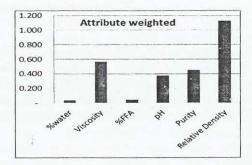
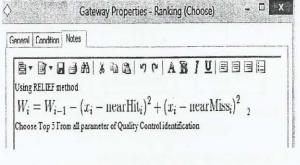
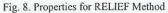


Fig. 7. Attribute Weighted Quality of Esterification

With RELIEF method we found the parameter that close related to quality is Relative Density, Purity, pH and Viscosity as the algorithm properties to explain this method as in Fig. 8. we identified quality parameter we are using optical sensors with real time data acquisition that connected to several quality parameter. And for the sequence of flow mixing as a process of production Glycerol Ester and Task properties for setting temperature was in Fig. 9 and Fig. 10.





-	Source	1	Destination	
	įb	lixing]	Mixing Oleic Acid	
		< <sequence flow="">></sequence>		
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aral Co	ndition Notes			ii
s:				
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4- [3-63613	AB X Y P	Ln 1, Col 1	
		as esterification		
Stea			LAAR ARADES	
	mixing at tempe	erature 200-300 00	(1020-2020L)	

Fig. 9. Sequence Flow Mixing Oleic Acid

🗊 Task Properties - Setting Temperature Esterification Reaction (S., 👘 🗖 💌

Dependenci	es	Traceability Link	cs	Version Info
General	Implementation	Notes	Rules	Related Diagrams
Name:	Setting Temperature Es	sterification Read	tion	
Code:	Setting_Temperature_E	sterification_Rea	action	
Comment:	Units: Celcius Degree	and the second		
Stereotype:	Script Task			- •
Organization unit	& <none></none>			v u 3 m
Timeout		D	uration:	
Composite status:	O Decomposed proces	ss 🔘 Atomic ti	ask Reusal	ole process
	1			Sector Sector Sector
Number ID:				
Number ID: Loop characteristics:	<none></none>			✓ Compensation
	<none></none>			

Fig. 10. Task Properties Setting Temperature

IV. ANALYSIS AND DESIGN PRODUCTION SYSTEM OF GLYCEROL ESTER

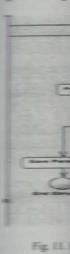
A. BPM and Process Modelling

We refer to a Business Process (BP) as "a collection of related and structured activities undertaken by one or more organizations in order to pursue some particular goal. Within an organization a BP results in the provisioning of services or in the production of goods for internal or external stakeholders. Moreover BPs are often interrelated since the execution of a BP often results in the activation of related BPs within the same or other organizations [15]. BPM supports BP experts that providing methods, techniques, and software to model, implement, execute and optimize BPs which involve humans, software applications, documents and other sources of information

This work had clearly shown that BP modeling has been identified as a fundamental phase in BP techniques which can help organizations to implement high-quality BPs, and to increase process modeling efficiency, has become an highly attractive topic both for industries and for the academy, to the best of our knowledge none of them introduces and supports formal verification techniques., such as the BPMN 2.0 [16]. The primary goal of BPMN is to

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provide a stan off business a imployed BPM and represent means a clear o the system and of the BPMON business process process concept compresention) esterification a a BPMON diago applicin the prointernet in Fig.



For data mesurement in optical sense andy state of inpured the isting proces uting time attrol us in Fi

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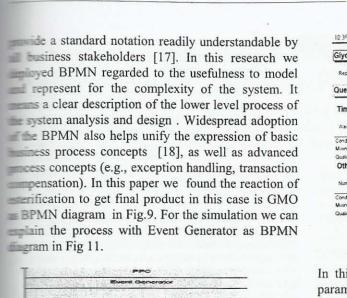


Related Diagrams

ICTION SYSTEM OF

Process (BP) as "a mactured activities izations in order to an organization a services or in the services or in the mal or external often interrelated ten results in the the same or other BP experts that software to model, BPs which involve cuments and other

shown that BP fundamental phase organizations to increase process highly attractive academy, to the introduces and ues., such as the of BPMN is to



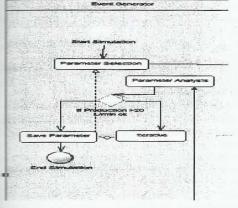


Fig. 11. BPMN Event Generator for Simulation

V. COMPUTATIONAL EXPERIMENT

A Result and Discussion

For data acquisition we are using online data measurement interfaced with SQL database and inputs by optical sensors. From the RTS that collected after seady state condition in process production. We compared the performance of the system between existing process and using SO, we get lower average maiting time in process condensation and quality control as in Fig. 12 and Fig. 13.

Replications: 1	Time Units:	Hours			
Queue					
Time					
Waiting Time		Average	Half Width	Moimum Value	Maria
Condensation.Queue		3.2168	(Insufficient)	1,6981	5.2
Miking Queue		2 5495	(Insufficient)	2,5495	25
Quality Control Queue		4.6514	(Insufficient)	4.6514	4.6
Other					-
Number Waiting		Average	Heif Width	Minimum Value	Maxim
Condensation Queue		6.7977	(Insufficient)	2,0000	12.0
Mining Queue		2.3919	(Insufficient)	1.0000	4.0
Chality Control Queue		1.2061	(Insufficient)	0.00	2.0

Fig. 12.Output Existing Process

Category Overview 10 35 45PM June 9 2014 Glycerol MonoOleat Optimize System Replicators Queue Time Wating Time Hatting 5314 Condensation Queue 3 2066 (Insufficient) 2914 Insufficient Mixing Queue 3 6000 2 3829 Quality Control Queue 4 4547 4 4543 Other Number Waiting Condensation Dueue 6 4628 2 0000 (Insufficient Mirang Queue 2 5110 Insufficient 1.0000 Quality Control Queue 1 2596



In this research we identify the effect of controlled parameter, consist of: temperature, baffle rotation speed and volume production for this research we have collected 100 data from production process as the sample of data in Table. II to find the range of SO for best parameter in production system

Table II. Sample of Production Data

Temperature (C)	Rotation Speed (RPM)	Volume Production(L)	Quality
240	300	28	Good
260	300	27	Good
260	350	29	Good
250	400	30	Good

B.Verification Model

Computerized model verification ensures that the computer programming and implementation of the conceptual like modelling the production system GE using Power Designer. When a simulation language is used, verification is primarily concerned with ensuring that an error free simulation language has been used, that the simulation language has been properly implemented on the computer that a tested (for correctness) pseudo random number event generator has been properly implemented and building diagram of BPMN, and the model has been programmed correctly in the simulation language [19]. In this case verification is primarily concerned with determining that the simulation real time functions (e.g., the timeflow mechanism, pseudo random number generator, and random variate generators) and the computer model have been programmed and implemented correctly [20]. With Power Designer we verify the model with error checking as captured in Fig. 14. If the result has shown 0 error and 0 warning, it means the flow of the sequence and interaction of data flow between all swimlane is correct.

Derror(s), 0 warning(s). The Business Process Model is correct, no errors were found.

Fig. 14. Error Checking Report in Power Designer

VI. CONCLUSION

The modelling of a real time simulation model of production system of glycerol esterification with self optimization contribute to support the production system of GMO. The analysis of the model was described for lower level process detailed in BPMN 2.0 diagram. With those diagram we found the relationship and interaction between stakeholders and clearly used for the simulation to improve the performance system. Verification of the model ensured implementation of the conceptual model. As a result of zero error checking and the RTS run as well. The experiments showed that the evaluation of the proposed system such as temperature between at range of 240-260 °C, baffle rotation speed between at range 300-400 RPM and volume at range 25-30 L for each batch .Compared with the previous works only set in a fixed value at 250 °C, 350 RPM and 24L. In future work, it is recommended to accelerate the whole process including to re-structure the real time data acquisition system.

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